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(54) **Process for preparing vinyl polymer**

(57) A vinyl polymer having a controlled molecular weight and narrow molecular weight distribution is prepared by polymerizing a vinyl monomer using an organic halide polymerization initiator in the presence of a cuprous compound catalyst in a solvent containing an organic compound having a dielectric constant of at least 10 at 25°C, or by polymerizing a vinyl monomer using an organic halide polymerization initiator in the presence of a cuprous compound catalyst and also a specific 1,10-phenanthroline compound.

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Description

BACKGROUND OF THE INVENTION

5 Field of the Invention

The present invention relates to a process for preparing a vinyl polymer having a controlled molecular weight and a narrow molecular weight distribution.

10 Description of the Prior Art

Molecular weights and molecular weight distributions of polymers have large influences on properties, such as flow properties, of the polymers. Thus, it is very important to prepare polymers having controlled molecular weights and narrow molecular weight distributions for controlling the properties of the prepared polymers and compositions comprising such the polymers.

A method for the easy preparation of a vinyl polymer having a controlled molecular weight and narrow molecular weight distribution, which is disclosed in J. Am. Chem. Soc., 117, 5614-5615 (1995), Macromolecules, 28, 7901-7910 (1995) and the like, comprises living radically polymerizing a vinyl monomer using an organic halide as a polymerization initiator and a monovalent copper complex which is obtained from a cuprous halide and an electron donating compound such as 2,2'-bipyridyl compounds. This process provides the polymer having the controlled molecular weight and narrow molecular weight distribution when the monomer is styrene, methyl acrylate, etc.

However, the molecular weight distributions of the vinyl polymers prepared by the above process are not still satisfactorily narrow. In particular, the molecular weight distributions of the vinyl polymers are slightly broad when this method is used for polymerizing acrylates (e.g. butyl acrylate, hexyl acrylate, 2-ethylhexyl acrylate, etc.), or methacrylates (e.g. methyl methacrylate, ethyl methacrylate, etc.).

Accordingly, it has been desired to provide a process for preparing vinyl polymers having narrower molecular weight distributions.

SUMMARY OF THE INVENTION

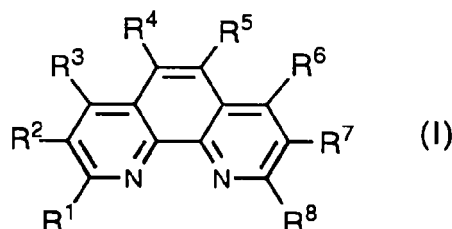
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An object of the present invention is to provide a process for preparing a vinyl polymer which has a controlled molecular weight and a narrower molecular weight distribution than the conventional vinyl polymers.

According to the first aspect, the present invention provides a process for preparing a vinyl polymer comprising polymerizing a vinyl monomer using an organic halide as a polymerization initiator in the presence of a cuprous compound as a catalyst in a solvent comprising an organic compound having a dielectric constant of at least 10 at 25°C.

According to the second aspect, the present invention provides a process for preparing a vinyl polymer comprising polymerizing a vinyl monomer using an organic halide as a polymerization initiator in the presence of a cuprous compound as a catalyst and a 1,10-phenanthroline compound of the formula (I):

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wherein R¹, R², R³, R⁴, R⁵, R⁶, R⁷ and R⁸ are the same or different and represent a hydrogen atom, an alkyl group having 1 to 10 carbon atoms, an aryl group having 6 to 10 carbon atoms or an aralkyl group having 7 to 10 carbon atoms.

DETAILED DESCRIPTION OF THE INVENTION

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The process of the present invention uses an organic halide as a polymerization initiator. The kind of the organic halide is not limited, and any halide which is used as a polymerization initiator for vinyl monomers may be used. Examples of such the organic halide are carbon tetrachloride, carbon tetrabromide, allyl chloride, allyl bromide, allyl iodide,

xylene derivatives (e.g. α,α' -dichloro-o-, m- or p-xylene, α,α' -dibromo-o-, m- or p-xylene, etc.), benzene derivatives (e.g. o-, m- or p-bis(α -chloroethyl)benzene, o-, m- or p-bis(α -bromoethyl)benzene, etc.), α -chloroacetates (e.g. methyl α -chloroacetate, ethyl α -chloroacetate, etc.), α,α -dichloroacetates (e.g. methyl α,α -dichloroacetate, ethyl α,α -dichloroacetate, etc.), α,α,α -trichloroacetates (e.g. methyl α,α,α -trichloroacetate, ethyl α,α,α -trichloroacetate, etc.), α -chloropropionates (e.g. methyl α -chloropropionate, ethyl α -chloropropionate, etc.), α -chloroisobutyrate (e.g. methyl α -chloroisobutyrate, ethyl α -isobutyrate, etc.), α -bromoacetates (e.g. methyl α -bromoacetate, ethyl α -bromoacetate, etc.), α,α -dibromoacetates (e.g. methyl α,α -dibromoacetate, ethyl α,α -dibromoacetate, etc.), α,α,α -tribromoacetates (e.g. methyl α,α,α -tribromoacetate, ethyl α,α,α -tribromoacetate, etc.), α -bromopropionates (e.g. methyl α -bromopropionate, ethyl α -bromopropionate, etc.), α -bromoisobutyrate (e.g. methyl α -bromoisobutyrate, ethyl α -bromoisobutyrate, etc.), and the like. These organic halides may be used independently or in admixture of two or more of them.

The amount of the polymerization initiator may be substantially the same as that in the conventional processes.

The process of the present invention uses a cuprous compound as a catalyst. The kind of the cuprous compound is not limited. Examples of the cuprous compound are cuprous chloride, cuprous bromide, cuprous iodide, cuprous cyanide, and the like.

The amount of the cuprous compound may be the same as in the conventional processes.

The cuprous compound is preferably used together with an electron donating compound. The kind of the electron donating compound is not limited. Examples of the electron donating compound are nitrogen atom-containing heterocyclic compounds such as bipyridyl (bipyridine) compounds (e.g. 2,2'-bipyridyl, 4,4'-dimethyl-2,2'-bipyridyl, etc.), phenanthroline compounds (e.g. 1,10-phenanthroline, 4,7-dimethyl-1,10-phenanthroline, 5,6-dimethyl-1,10-phenanthroline, 3,4,7,8-tetramethyl-1,10-phenanthroline, etc.), and the like.

The amount of the electron donating compound is usually between 0.5 and 5 moles, preferably between 2 and 3 moles, per one mole of the cuprous compound.

The kind of the vinyl monomer which is polymerized by the process of the present invention is not limited. Examples of the vinyl monomer are (meth)acrylates (e.g. methyl (meth)acrylate, ethyl (meth)acrylate, n-propyl (meth)acrylate, isopropyl (meth)acrylate, n-butyl (meth)acrylate, isobutyl (meth)acrylate, tert.-butyl (meth)acrylate, n-pentyl (meth)acrylate, n-hexyl (meth)acrylate, cyclohexyl (meth)acrylate, n-heptyl (meth)acrylate, n-octyl (meth)acrylate, 2-ethylhexyl (meth)acrylate, nonyl (meth)acrylate, decyl (meth)acrylate, dodecyl (meth)acrylate, etc.), styrene and its derivatives (e.g. 2-, 3- or 4-methylstyrene, 2-, 3- or 4-chlorostyrene, 2-, 3- or 4-(chloromethyl)styrene, 2-, 3- or 4-methoxystyrene, 2-, 3- or 4-(methoxycarbonyl)styrene, α -methylstyrene, etc.), maleic anhydride, and the like. They may be used independently or in admixture of two or more of them.

In one preferred embodiment of the process of the present invention, the vinyl monomer is polymerized in a solvent comprising an organic compound having a dielectric constant of at least 10 measured at 25°C.

The kind of such the organic compound is not limited.

A preferred example of such the organic compound is a carbonyl compound of the formula (II):



wherein R^9 and R^{10} are the same or different and represent a hydrogen atom, an alkyl group having 1 to 10 carbon atoms, an aryl group having 6 to 10 carbon atoms or an aralkyl group having 7 to 10 carbon atoms, or R^9 and R^{10} forms a cyclic alkyl group together with the carbonyl group.

Specific examples of the carbonyl compound of the formula (II) are acyclic aliphatic ketones (e.g. acetone, 2-butanone, 2- or 3-pentanone, 2-hexanone, 2-heptanone, 4-methyl-2-pentanone, etc.), cyclic aliphatic ketones (e.g. cyclohexanone, 2-, 3- or 4-methylcyclohexanone, etc.), aromatic ketones (e.g. acetophenone, 2-, 3- or 4-methylacetophenone, etc.), and the like.

Another example of such the organic compound is a nitro compound of the formula (III):



wherein R^{11} is an alkyl group having 1 to 10 carbon atoms, an aryl group having 6 to 10 carbon atoms or an aralkyl group having 7 to 10 carbon atoms.

Specific examples of the nitrocompound of the formula (III) are nitromethane, nitroethane, nitropropane, nitrobenzene, and the like.

A further example of such the compound is a nitrile compound of the formula (IV):



wherein R^{11} is the same as defined above.

Specific examples of the nitrile compound of the formula (IV) are acetonitrile, propionitrile, benzonitrile, and the like.

A still further examples of such the organic compound is an alcohol of the formula (V):



5 wherein R^{12} is a hydrogen atom, an alkyl group having 1 to 10 carbon atoms, an aryl group having 6 to 10 carbon atoms or an aralkyl group having 7 to 10 carbon atoms.

Specific examples of the alcohol of the formula (V) are methanol, ethanol, 1- or 2-propanol, 1-butanol, cyclohexanol, benzyl alcohol, and the like.

10 The carbonyl compound (II), nitro compound (III), nitrile compound (IV) and alcohol compound (V) may be used independently or in admixture of two or more of them.

The organic compound having the dielectric constant of at least 10 measured at 25°C may be used together with at least one other solvent.

The kind of the other solvent is not limited. Preferable example of the other solvent are organic compounds such as hexane, toluene, ethyl acetate, tetrahydrofurane, etc.

15 The amount of the organic compound having the dielectric constant of at least 10 at 25°C is preferably between 10 to 100 vol. % of the whole solvent, when the other solvent is used. If the amount of such the organic solvent is less than 10 vol. %, the obtained vinyl polymer may have a wide molecular weight distribution.

In the process of the present invention, the whole volume of the solvent is not limited. Preferably, the total amount of the solvent is between 0.5 and 10 times the volume of the vinyl monomer for achieving the suitable reaction rate.

20 In the present invention, the polymerization temperature is adequately selected according to the kind of the vinyl monomer, and other conditions. In general, the polymerization temperature is between 60 and 150°C.

In another preferred embodiment of the present invention, the polymerization is carried out in the presence of a 1,1-phenanthroline compound of the above formula (I).

25 When the vinyl monomer is polymerized in the presence of the phenanthroline compound of the formula (I), the obtained vinyl polymer has the controlled molecular weight and narrow molecular weight distribution.

Unexpectedly, it has been found that the 1,10-phenanthroline compound (I) achieves the higher polymerization rate than the conventional electron donating compounds which coordinate on a cuprous catalyst, such as 2,2'-bipyridyl compounds. The higher polymerization rate is advantageous from the economical point of view in the industrial scale production of the vinyl polymers.

30 When the polymerization is carried out in the presence of the 1,10-phenanthroline compound (I), the organic compound having the dielectric constant of at least 10 at 25°C is preferably used as the solvent, although other solvent may be used.

Specific examples of the 1,10-phenanthroline compound (I) are 1,10-phenanthroline, 2-, 3-, 4- or 5-methyl-1,10-phenanthroline, 2,3-, 2,4-, 2,5-, 2,6-, 2,7-, 2,8-, 3,4-, 3,5-, 3,6-, 3,7-, 3,8-, 4,5-, 4,6-, 4,7- or 5,6-dimethyl-1,10-phenanthroline, 2,3,4-, 2,3,5-, 2,3,6-, 2,3,7-, 2,3,8-, 3,4,5-, 3,4,6-, 3,4,7-, 3,5,8- or 4,5,7-trimethyl-1,10-phenanthroline, 3,4,7,8- or 4,5,6,7-1,10-phenanthroline, 4,7-diphenyl-1,10-phenanthroline, 4,7-benzyl-1,10-phenanthroline, and the like. They may be used independently or in admixture of two or more of them.

The amount of the 1,1-phenanthroline compound of the formula (I) is usually between 0.5 and 5 moles, preferably between 2 and 3 moles, per one mole of the cuprous compound.

40 The vinyl polymer prepared by the process of the present invention usually has a number average molecular weight of between 500 and 100,000. The molecular weight distribution achieved by the process of the present invention is usually between 1 and 1.5 in terms of M_w/M_n .

45 The vinyl polymer prepared by the process of the present invention is expected to have a smaller viscosity than vinyl polymers which are obtained by the conventional processes and have the same backbone and molecular weight, since it has the narrow molecular weight distribution.

EXAMPLES

50 The present invention will be illustrated by the following Examples, which will not limit the scope of the present invention in any way.

In the Examples, the following commercially available reagents were used without purification:

Methyl acrylate: available from TOKYO KASEI, guaranteed reagent;

Butyl acrylate: available from WAKO JUNYAKU, purity of 99.9 %;

55 Ethyl α -bromopropionate: available from TOKYO KASEI;

α,α' -Dibromo-p-xylene: available from WAKO JUNYAKU, guaranteed reagent;

2,2'-Bipyridyl, 1,10-phenanthroline, 4,7-dimethyl-1,10-phenanthroline, 5,6-dimethyl-1,10-phenanthroline, and 3,4,7,8-tetramethyl-1,10-phenanthroline: all available from TOKYO KASEI.

Also the following commercially available solvents were used without purification:

Toluene: available from WAKO JUNYAKU, guaranteed reagent;
 Ethyl acetate: available from WAKO JUNYAKU, guaranteed reagent;
 5 Acetone and 4-methyl-2-pentanone: both available from WAKO JUNYAKU, guaranteed reagent;
 Ethanol: available from WAKO JUNYAKU, guaranteed reagent;
 Nitroethane: available from WAKO JUNYAKU, extra pure grade reagent;
 Acetonitrile: available from WAKO JUNYAKU, guaranteed reagent;
 10 Benzonitrile: available from ISHIZU SEIYAKU, guaranteed reagent.

Example 1

In a pressure-resistant 30 ml glass reactor, butyl acrylate (10 ml, 9.94 g, 69.8 mmol), α, α' -dibromo-p-xylene (370 mg, 1.4 mmol), cuprous bromide (200 mg, 1.4 mmol), 2,2'-bipyridyl (652 mg, 4.2 mmol) and acetone (dielectric constant of 20.70 at 25°C) (10 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 3 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (4.26 g) was obtained. The polymer yield was 47.6 %.

The number average molecular weight of the obtained polymer was 3900, and the polydispersity (Mw/Mn) was 1.17, both measured by GPC (as converted to polystyrene).

Example 2

In a pressure-resistant 30 ml glass reactor, methyl acrylate (3.1 ml, 3.0 g, 34.9 mmol), α, α' -dibromo-p-xylene (185 mg, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 2,2'-bipyridyl (326 mg, 2.1 mmol) and 4-methyl-2-pentanone (dielectric constant of 13.11 at 25°C) (3.14 ml) were charged, and dissolved oxygen was purged by bubbling nitrogen gas for 10 minutes. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 0.5 hour. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(methyl acetate) (2.07 g) was obtained. The polymer yield was 68.8 %.

The number average molecular weight of the obtained polymer was 3900, and the polydispersity (Mw/Mn) was 1.31, both measured by GPC (as converted to polystyrene).

Example 3

In a pressure-resistant 30 ml glass reactor, butyl acrylate (5 ml, 4.47 g, 34.9 mmol), α, α' -dibromo-p-xylene (185 mg, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 2,2'-bipyridyl (326 mg, 2.1 mmol) and acetonitrile (dielectric constant of 36.0 at 25°C) (5 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 150°C and reacted for 9 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (1.41 g) was obtained. The polymer yield was 31.5 %.

The number average molecular weight of the obtained polymer was 2800, and the polydispersity (Mw/Mn) was 1.21, both measured by GPC (as converted to polystyrene).

Example 4

In a pressure-resistant 30 ml glass reactor, butyl acrylate (5 ml, 4.47 g, 34.9 mmol), ethyl α -bromopropionate (0.090 ml, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 2,2'-bipyridyl (326 mg, 2.1 mmol) and acetonitrile (5 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 5 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pres-

sure, and poly(butyl acrylate) (2.95 g) was obtained. The polymer yield was 66.0 %.

The number average molecular weight of the obtained polymer was 3600, and the polydispersity (Mw/Mn) was 1.13, both measured by GPC (as converted to polystyrene).

5 Example 5

In a pressure-resistant 30 ml glass reactor, butyl acrylate (5 ml, 4.47 g, 34.9 mmol), α,α' -dibromo-p-xylene (185 mg, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 2,2'-bipyridyl (326 mg, 2.1 mmol), acetonitrile (5 ml) and ethyl acetate (dielectric constant of 6.02 at 25°C) (2.5 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 6 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (2.83 g) was obtained. The polymer yield was 63.3 %.

The number average molecular weight of the obtained polymer was 5100, and the polydispersity (Mw/Mn) was 1.15, both measured by GPC (as converted to polystyrene).

Example 6

In a pressure-resistant 30 ml glass reactor, butyl acrylate (5 ml, 4.47 g, 34.9 mmol), α,α' -dibromo-p-xylene (185 mg, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 2,2'-bipyridyl (326 mg, 2.1 mmol), acetonitrile (1 ml) and ethyl acetate (4 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 2 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (3.79 g) was obtained. The polymer yield was 84.8 %.

The number average molecular weight of the obtained polymer was 5700, and the polydispersity (Mw/Mn) was 1.26, both measured by GPC (as converted to polystyrene).

Example 7

In a pressure-resistant 30 ml glass reactor, butyl acrylate (5 ml, 4.47 g, 34.9 mmol), ethyl α -bromopropionate (0.090 ml, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 2,2'-bipyridyl (326 mg, 2.1 mmol) and benzonitrile (dielectric constant of 25.20 at 25°C) (5 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 2 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (2.48 g) was obtained. The polymer yield was 55.5 %.

The number average molecular weight of the obtained polymer was 3600, and the polydispersity (Mw/Mn) was 1.16, both measured by GPC (as converted to polystyrene).

Example 8

In a pressure-resistant 30 ml glass reactor, butyl acrylate (5 ml, 4.47 g, 34.9 mmol), ethyl α -bromopropionate (0.090 ml, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 2,2'-bipyridyl (326 mg, 2.1 mmol) and nitroethane (dielectric constant of 28.06 at 30°C) (5 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 6 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (1.97 g) was obtained. The polymer yield was 44.1 %.

The number average molecular weight of the obtained polymer was 2000, and the polydispersity (Mw/Mn) was 1.23, both measured by GPC (as converted to polystyrene).

Example 9

In a pressure-resistant 30 ml glass reactor, methyl acrylate (3.1 ml, 3.0 g, 34.9 mmol), α,α' -dibromo-p-xylene (185 mg, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 2,2'-bipyridyl (326 mg, 2.1 mmol), acetonitrile (0.63 ml) and ethyl acetate (2.51 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 2 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(methyl acetate) (2.09 g) was obtained. The polymer yield was 70.0 %.

The number average molecular weight of the obtained polymer was 4300, and the polydispersity (Mw/Mn) was 1.18, both measured by GPC (as converted to polystyrene).

Example 10

In a pressure-resistant 30 ml glass reactor, methyl acrylate (3.1 ml, 3.0 g, 34.9 mmol), α,α' -dibromo-p-xylene (185 mg, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 2,2'-bipyridyl (326 mg, 2.1 mmol) and ethanol (dielectric constant of 24.55 at 25°C) (0.63 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 2 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(methyl acetate) (2.01 g) was obtained. The polymer yield was 67.0 %.

The number average molecular weight of the obtained polymer was 3600, and the polydispersity (Mw/Mn) was 1.37, both measured by GPC (as converted to polystyrene).

Comparative Example 1

In a pressure-resistant 30 ml glass reactor, butyl acrylate (5 ml, 4.47 g, 34.9 mmol), α,α' -dibromo-p-xylene (185 mg, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol) and 2,2'-bipyridyl (326 mg, 2.1 mmol) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 1 hour. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (4.45 g) was obtained. The polymer yield was 99.6 %.

The number average molecular weight of the obtained polymer was 6300, and the polydispersity (Mw/Mn) was 1.75, both measured by GPC (as converted to polystyrene).

Comparative Example 2

In a pressure-resistant 30 ml glass reactor, butyl acrylate (5 ml, 4.47 g, 34.9 mmol), α,α' -dibromo-p-xylene (185 mg, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 2,2'-bipyridyl (326 mg, 2.1 mmol) and ethyl acetate (dielectric constant of 6.02) (5 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 6 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (4.31 g) was obtained. The polymer yield was 96.4 %.

The number average molecular weight of the obtained polymer was 6300, and the polydispersity (Mw/Mn) was 1.77, both measured by GPC (as converted to polystyrene).

Comparative Example 3

In a pressure-resistant 30 ml glass reactor, butyl acrylate (5 ml, 4.47 g, 34.9 mmol), α,α' -dibromo-p-xylene (185 mg, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 2,2'-bipyridyl (326 mg, 2.1 mmol) and toluene (dielectric constant of 2.38 at 25°C) (5 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 4 hours. The reaction mixture was diluted with ethyl acetate, and

washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (4.41 g) was obtained. The polymer yield was 98.7 %.

5 The number average molecular weight of the obtained polymer was 5800, and the polydispersity (M_w/M_n) was 1.92, both measured by GPC (as converted to polystyrene).

The results of Examples 1 through 10 and Comparative Examples 1, 2 and 3 are summarized in Table 1, in which "BA", "MA", "Bromoxylene", "Bromoester" and "Bipyridyl" mean butyl acrylate, methyl acrylate, α,α' -dibromo-p-xylene, ethyl α -bromopropionate, and 2,2'-bipyridyl, respectively.

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Table 1

Ex. No.	Monomer (mmol)	Initiator (mmol)	Catalysts (mmol)	Solvent (ml)	Reaction temp. (°C)	Reaction time (hr)	Polymer	
							Yield (%)	Mw/Mn
1	BA (69.8)	Bromoxylene (1.4)	CuBr/bipyridyl (1.4/4.2)	Acetone (10)	130	3	47.6	1.17
2	MA (34.9)	Bromoxylene (0.7)	CuBr/bipyridyl (0.7/2.1)	4-Methyl-2-pentanone (3.14)	130	0.5	68.8	1.31
3	BA (34.9)	Bromoxylene (0.7)	CuBr/bipyridyl (0.7/2.1)	Acetonitrile (5)	150	9	31.5	1.21
4	BA (34.9)	Bromoester (0.7)	CuBr/bipyridyl (0.7/2.1)	Acetonitrile (5)	130	5	66.0	1.13
5	BA (34.9)	Bromoxylene (0.7)	CuBr/bipyridyl (0.7/2.1)	Acetonitrile/ethyl acetate (2.5/2.5)	130	6	63.3	1.15
6	BA (34.9)	Bromoxylene (0.7)	CuBr/bipyridyl (0.7/2.1)	Acetonitrile/ethyl acetate (1/4)	130	2	84.8	1.26
7	BA (34.9)	Bromoester (0.7)	CuBr/bipyridyl (0.7/2.1)	Benzonitrile (5)	130	2	55.5	1.16
8	BA (34.9)	Bromoester (0.7)	CuBr/bipyridyl (0.7/2.1)	Nitroethane (5)	130	6	44.1	1.23
9	MA (34.9)	Bromoxylene (0.7)	CuBr/bipyridyl (0.7/2.1)	Acetonitrile/ethyl acetate (0.63/2.51)	130	2	70.0	1.18
10	MA (34.9)	Bromoxylene (0.7)	CuBr/bipyridyl (0.7/2.1)	Ethanol/ethyl acetate (0.63/2.51)	130	2	67.0	1.37

Table 1 (continued)

Com. Ex. No.	Monomer (mmol)	Initiator (mmol)	Catalysts (mmol)	Solvent (ml)	Reaction temp. (°C)	Reaction time (hr)	Polymer	
							Yield (%)	Mw/Mn
C. 1	BA (34.9)	Bromoxylene (0.7)	CuBr/bipyridyl (0.7/2.1)	- - -	130	1	99.6	1.75
C. 2	BA (34.9)	Bromoxylene (0.7)	CuBr/bipyridyl (0.7/2.1)	Ethyl acetate (5)	130	6	96.4	1.77
C. 3	BA (34.9)	Bromoxylene (0.7)	CuBr/bipyridyl (0.7/2.1)	Toluene (5)	130	4	98.7	1.92

As seen from the comparison of the results of Examples 1 through 10 and those of Comparative Examples 1, 2 and 3, the polymers obtained by the polymerization in the solvents having the high dielectric constant had the narrow

molecular weight distribution (Mw/Mn).

Example 11

In a pressure-resistant 30 ml glass reactor, butyl acrylate (5 ml, 4.47 g, 34.9 mmol), α,α' -dibromo-p-xylene (185 mg, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 1,10-phenanthroline (378 mg, 2.1 mmol) and acetonitrile (5 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 6 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (2.27 g) was obtained. The polymer yield was 50.8 %.

The number average molecular weight of the obtained polymer was 3500, and the polydispersity (Mw/Mn) was 1.21, both measured by GPC (as converted to polystyrene).

Example 12

In a pressure-resistant 30 ml glass reactor, butyl acrylate (2.5 ml, 2.24 g, 17.5 mmol), α,α' -dibromo-p-xylene (93 mg, 0.35 mmol), cuprous bromide (50 mg, 0.35 mmol), 4,7-dimethyl-1,10-phenanthroline (219 mg, 1.05 mmol) and acetonitrile (2.5 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 3 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (0.54 g) was obtained. The polymer yield was 24.1 %.

The number average molecular weight of the obtained polymer was 2100, and the polydispersity (Mw/Mn) was 1.36, both measured by GPC (as converted to polystyrene).

Example 13

In a pressure-resistant 30 ml glass reactor, butyl acrylate (2.5 ml, 2.24 g, 17.5 mmol), α,α' -dibromo-p-xylene (93 mg, 0.35 mmol), cuprous bromide (50 mg, 0.35 mmol), 5,6-dimethyl-1,10-phenanthroline (219 mg, 1.05 mmol) and acetonitrile (2.5 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 5 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (2.66 g) was obtained. The polymer yield was 118.8 %.

The number average molecular weight of the obtained polymer was 7400, and the polydispersity (Mw/Mn) was 1.37, both measured by GPC (as converted to polystyrene).

Example 14

In a pressure-resistant 30 ml glass reactor, butyl acrylate (5 ml, 4.47 g, 34.9 mmol), α,α' -dibromo-p-xylene (185 mg, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 3,4,7,8-tetramethyl-1,10-phenanthroline (496 mg, 2.1 mmol) and acetonitrile (5 ml) were charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 6 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (4.38 g) was obtained. The polymer yield was 98.0 %.

The number average molecular weight of the obtained polymer was 7800, and the polydispersity (Mw/Mn) was 1.49, both measured by GPC (as converted to polystyrene).

Example 15

In a pressure-resistant 30 ml glass reactor, butyl acrylate (5 ml, 4.47 g, 34.9 mmol), α,α' -dibromo-p-xylene (185 mg, 0.70 mmol), cuprous bromide (100 mg, 0.70 mmol), 2,2'-bipyridyl (326 mg, 2.1 mmol) and acetonitrile (5 ml) were

charged, and the interior of the reactor was evacuated three times to purge dissolved oxygen. Then, the reactor was sealed.

The mixture was heated to 130°C and reacted for 5 hours. The reaction mixture was diluted with ethyl acetate, and washed with 10 % hydrochloric acid three times and with a brine one time.

5 The organic layer was dried over anhydrous sodium sulfate, and the solvent was distilled off under reduced pressure, and poly(butyl acrylate) (0.65 g) was obtained. The polymer yield was 14.5 %.

The number average molecular weight of the obtained polymer was 1100, and the polydispersity (Mw/Mn) was 1.36, both measured by GPC (as converted to polystyrene).

10 The results of Examples 11 through 15 are summarized in Table 2, in which "Phenanthroline A" "Phenanthroline B", "Phenanthroline C", "Phenanthroline D" and "Bipyridyl" mean "1,10-phenanthroline, 4,7-dimethyl-1,10-phenanthroline, 5,6-dimethyl-1,10-phenanthroline, 3,4,7,8-tetramethyl-1,10-phenanthroline, and 2,2'-bipyridyl, respectively.

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Table 2

Ex. No.	Monomer (mmol)	Initiator (mmol)	Catalysts (mmol)	Solvent (ml)	Reaction temp. (°C)	Reaction time (hr)	Polymer	
							Yield (%)	Mw/Mn
11	BA (34.9)	Bromoxylene (0.7)	CuBr/phenanthroline A (0.7/2.1)	Acetonitrile (5)	130	6	50.8	1.21
12	BA (17.5)	Bromoxylene (0.35)	CuBr/phenanthroline B (0.35/1.05)	Acetonitrile (2.5)	130	3	24.1	1.36
13	BA (17.5)	Bromoxylene (0.35)	CuBr/phenanthroline C (0.35/1.05)	Acetonitrile (2.5)	130	5	111.8	1.37
14	BA (34.9)	Bromoxylene (0.7)	CuBr/phenanthroline D (0.7/2.1)	Acetonitrile (5)	130	6	98.0	1.49
15	BA (34.9)	Bromoxylene (0.7)	CuBr/bipyridyl (0.7/2.1)	Acetonitrile (5)	130	5	14.5	1.36

As seen from the results in Table 2, the use of the 1,10-phenanthroline compounds provided the polymers having the molecular weight distribution which is the same as or smaller than that achieved by the use of the bipyridyl compound. Furthermore, it is seen from the data of reaction time and polymer yield that the 1,10-phenanthroline com-

pounds achieved the higher polymerization reaction rates than the bipyridyl compound.

Claims

1. A process for preparing a vinyl polymer comprising polymerizing a vinyl monomer using an organic halide as a polymerization initiator in the presence of a cuprous compound as a catalyst in a solvent comprising an organic compound having a dielectric constant of at least 10 at 25°C.
2. A process according to claim 1, wherein said organic compound having the dielectric constant of at least 10 at 25°C is at least one compound selected from the group consisting of:

a compound of a carbonyl compound of the formula (II):



wherein R^9 and R^{10} are the same or different and represent a hydrogen atom, an alkyl group having 1 to 10 carbon atoms, an aryl group having 6 to 10 carbon atoms or an aralkyl group having 7 to 10 carbon atoms, or R^9 and R^{10} forms a cyclic alkyl group together with the carbonyl group; a nitro compound of the formula (III):



wherein R^{11} is an alkyl group having 1 to 10 carbon atoms, an aryl group having 6 to 10 carbon atoms or an aralkyl group having 7 to 10 carbon atoms; a nitrile compound of the formula (IV):

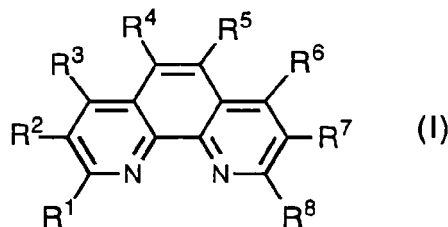


wherein R^{11} is the same as defined above; and an alcohol of the formula (V):



wherein R^{12} is a hydrogen atom, an alkyl group having 1 to 10 carbon atoms, an aryl group having 6 to 10 carbon atoms or an aralkyl group having 7 to 10 carbon atoms..

3. A process according to claim 1, wherein an amount of said organic compound having the dielectric constant of at least 10 at 25°C is between 10 to 100 vol. % of the whole solvent.
4. A process for preparing a vinyl polymer comprising polymerizing a vinyl monomer using an organic halide as a polymerization initiator in the presence of a cuprous compound as a catalyst and a 1,10-phenanthroline compound of the formula (I):



wherein R^1 , R^2 , R^3 , R^4 , R^5 , R^6 , R^7 and R^8 are the same or different and represent a hydrogen atom, an alkyl group having 1 to 10 carbon atoms, an aryl group having 6 to 10 carbon atoms or an aralkyl group having 7 to 10 carbon atoms.



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EUROPEAN SEARCH REPORT

Application Number

DOCUMENTS CONSIDERED TO BE RELEVANT			EP 97109952.8
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl. 6)
X	YOSHIKI NAKAGAWA et al. The Synthesis of End Functional Polymers by "Living" Radical Polymerization. Luisiana: Polymer Preprints. March 1996, Vol. 37, No. 1, pages 577-578, especially the whole document.	1,3	C 08 F 4/50 C 08 F 2/14
X, D	WANG, J.-S. Controlled/ "Living" Radical Polymerization. Halogen Atom Transfer Radical Polymerization Promoted by a Cu(I)/Cu(II) Redox Process. Macromolecules. November 1995, Vol. 28, No. 23, pages 7901-7910, especially abstract, experimental section.	1,3	
X, P	WO 96/30421 A1 (K. MATYJASZEWSKI et al.) 03 October 1996 (03.10.96), abstract, page 24, lines 11-13, page 26, lines 3-8, page 27, line 21- page 28, line 15, example 12.	1-4	TECHNICAL FIELDS SEARCHED (Int. Cl.6) B 01 J 31/00 C 08 F 2/00 C 08 F 4/00
X, P	WO 97/18247 A1 (CARNEGIE MELLON UNIVERSITY) 22 May 1997 (22.05.97), abstract, page 50, lines 4-10, page 53, line 17 - page 54, line 15, page 55, lines 16-23, example 4.	1-4	
The present search report has been drawn up for all claims			
Place of search VIENNA		Date of completion of the search 06-10-1997	Examiner PUSTERER
<p>CATEGORY OF CITED DOCUMENTS</p> <p>X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document</p> <p>T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family, corresponding document</p>			

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